

CHE 3214L Chemical Engineering Laboratory Investigations 1

Experiment Plan
(Form CHE 3214L-1)

Prepared and submitted by:

Gibson Jake C. Canama

Monica Claire L. Delco

Rhoel A. Talandron

Experiment : **Fluid in Pipes 2: Flow Regime and Pressure Drop**

Objectives of the Experiment

- 1) Determine the flow regime of a liquid at a given set of flow parameters
- 2) Determine the effect of mass flowrate to the pressure drop of a liquid for a given pipe
- 3) Compare the obtained experiment values to the calculated, simulator values.

Methodological Framework

Objective 1: Determine the flow regime of a liquid at a given set of flow parameters.

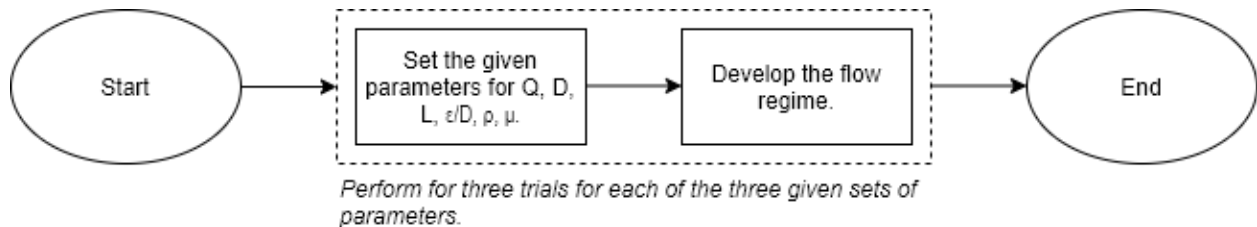


Figure 1. Methodological Framework for Objective 1

Objective 2: Determine the effect of mass flowrate to the pressure drop of a liquid for a given pipe.

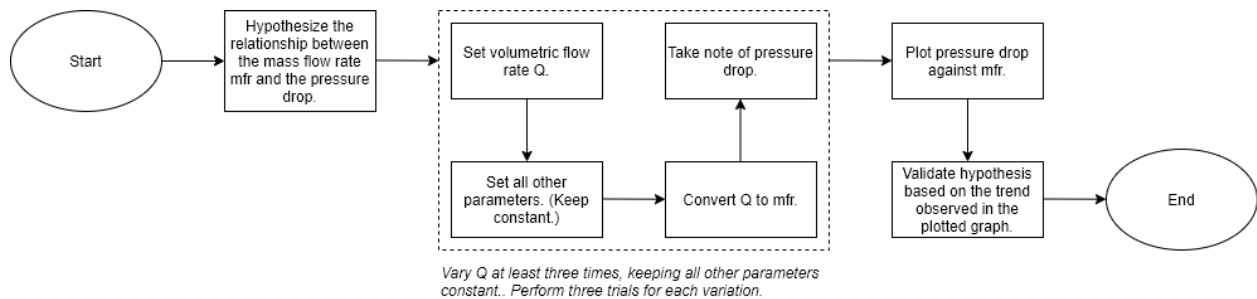


Figure 2. Methodological Framework for Objective 2

Objective 3: Compared the obtained experiment values to the calculated, simulator values.

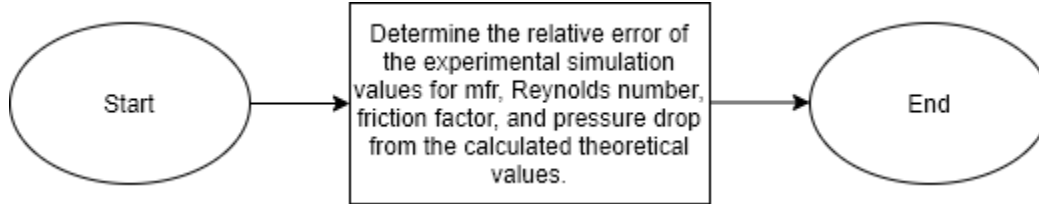


Figure 3. Methodological Framework for Objective 3

Materials, Measuring Apparatus & Equipment		
Material		Quantity
Liquid		Density Range: $500 \frac{kg}{m^3} - 1500 \frac{kg}{m^3}$ Viscosity Range: $1000 Pa.s - 1.5 Pa.s$
Equipment		Specifications
Pipe		Diameter Range: $1cm - 50cm$ Unknown Material Length Range: $0m - 100m$

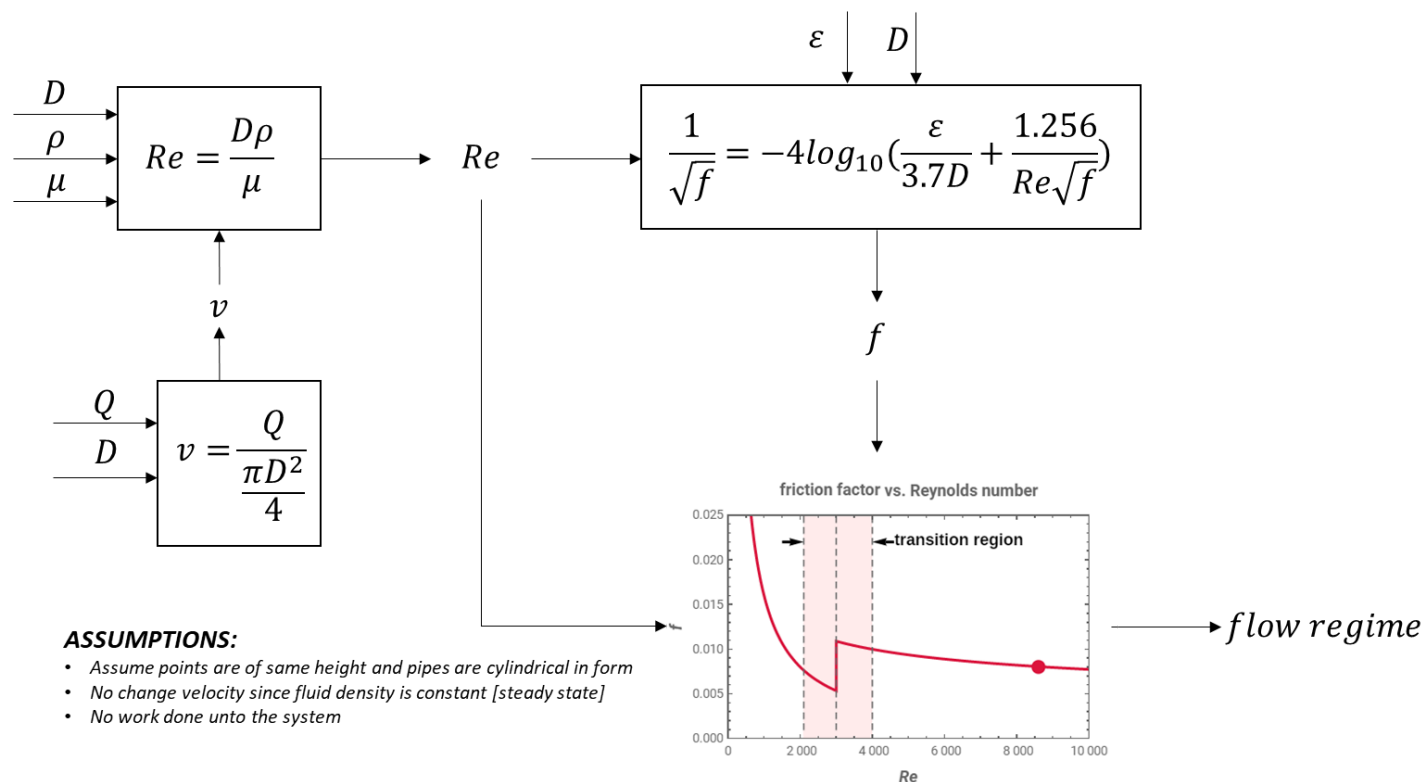
Task Plan		
Time	Task	Person Responsible
1:30-3:00	Pre-Laboratory Virtual Questioning	Canama
		Delco
		Talandron
3:00 – 3:10	Open Virtual Laboratory Link > Frictional Pressure Drop in Pipe Simulator	Canama Delco Talandron (Note: Each member shall do the procedures individually and simultaneously)
	Taking note of the Conditions for RUN 1*	
	Selection of Pipe Diameter	
	Selection of Pipe Length	
	Selection of Relative Roughness, $\frac{\epsilon}{D}$	
	Selection of Fluid Density and Viscosity	
	Selection of Volumetric Flow Rate	
	Reading and Recording of Mass Flow Rate, Reynold's Number, Friction Factor, and Pressure Drop from Simulator	
	Calculate the Mass Flow Rate, Reynold's Number, Friction Factor, and Pressure Drop using Given Data	
	Resetting the Simulation Set-up for Next Pipe Diameter Run	
3:10 – 3.20	Repetition of Procedures for RUN 2*	Canama Delco Talandron

		(Note: Each member shall do the procedures individually and simultaneously)
3:20 – 3:30	Repetition of Procedures for RUN 3*	Canama Delco Talandron (Note: Each member shall do the procedures individually and simultaneously)
3:30 – 4:00	Collection of Raw Data; Documentation Procedures; Plotting of Simulator and Calculated Data	Canama Delco Talandron
4:00 – 4:15	Analysis and Processing of Observed Mechanisms and Data Values from the Simulator	
4:15 – 4:30	Wrap-up of Discussions	

*The Selection of the Different Runs will be given by the Instructor herself.

Information Flow Diagram

Objective 1: Determine the flow regime of a liquid at a given set of flow parameters.



$$\Delta \left(\frac{P}{\rho} + gz + \frac{v^2}{2} \right) = \frac{-dW_{ao}}{dm} + F$$

ASSUMPTIONS:

- Assume points are of same height and pipes are cylindrical in form
- No change velocity since fluid density is constant [steady state]
- No work done unto the system

$$\frac{\Delta P}{\rho} = F$$

$$\Delta P = \rho f_D \frac{L}{D} \frac{v^2}{2}$$

$$F = f_D \frac{L}{D} \frac{v^2}{2}$$

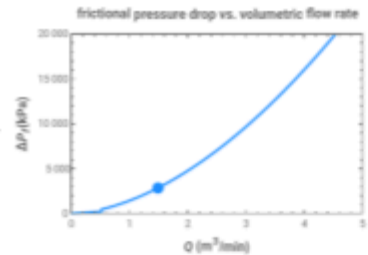
\uparrow \uparrow \uparrow \uparrow
 L D f_D

$$v = \frac{Q}{\frac{\pi D^2}{4}}$$

\uparrow \uparrow
 Q D

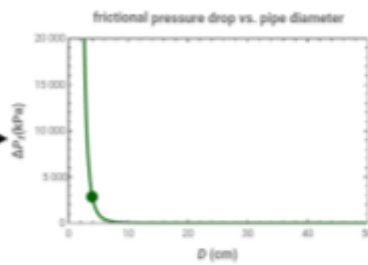
$$\dot{M} = Q\rho$$

ΔP



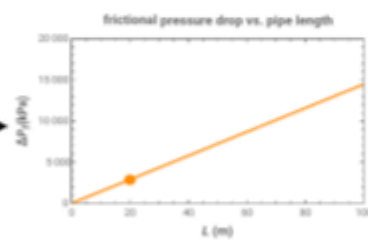
$\leftarrow Q$

Relation between



$\leftarrow D$

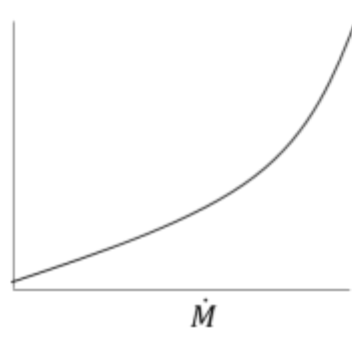
Relation between and



$\leftarrow L$

Relation between

ΔP



Relationship between and

Objective 2: Determine the effect of mass flowrate to the pressure drop of a liquid for a given pipe

Objective 3: Compare the Obtained Experiment Values to the Calculated, Simulator Values



$$\delta = \frac{|\Delta P - \Delta P_{expt}|}{\Delta P} \times 100\%$$

δ

Legend:

$g = \text{Acceleration due to Gravity} \left(\frac{m}{s^2} \right) = 9.81 \frac{m}{s^2}$

$Q = \text{Volumetric Flowrate} \left(\frac{m^3}{min} \right)$

$F = \text{Friction Term}$

$z = \text{height (cm)}$

$D = \text{Pipe Inner Diameter (cm)}$

$L = \text{Pipe Length (m)}$

$v = \text{Velocity} \left(\frac{m}{s} \right)$

$f_D = \text{Darcy - Weisbach Friction Factor}$

$\varepsilon = \text{Surface Roughness}$

$\rho = \text{Density of fluid (kg/m}^3\text{)}$

$\mu = \text{Viscosity of Fluid (Pa. s)}$

$Re = \text{Reynold's Number}$

$\Delta P_{\text{expt}} = \text{Experimental Pressure Drop from Simulator (kPa)}$

$\Delta P = \text{Pressure Drop (kPa)}$

$\delta = \text{Relative Error (\%)}$

$\dot{M} = \text{Mass Flowrate (kg/min)}$

CANAMA: Raw Data and Documentation

Table 1.1 Raw Data Set for Objective 1

Run	Q (m ³ /min)	D (cm)	L (m)	ϵ/D	ρ (kg/m ³)	μ (Pa.s)	Flow Regime (screenshot)
1	1	1	20	0.01	500	0.001	
2	2	2	40	0.02	750	0.01	
3	3	3	60	0.03	1000	0.1	

Table 1.2 Raw Data Set for Objective 2

Run	Q (m ³ /min)	D (cm)	L (m)	ϵ/D	ρ (kg/m ³)	μ (Pa.s)	mfr (kg/min)	ΔP_f (kPa)
1	1	1	20	0.01	500	0.01	500	854,729
2	2						1000	3,416,327
3	3						1500	7,684,792
4	4						2000	13,660,122
5	5						2500	21,342,319

Observations:

As the parameters increases in its value, the closer it is towards the transition region. Further, the point in the graph shows where the condition is situated in the Moody chart. Thus, it can be inferred, based on the value of Re, that the flow of the pipe is at turbulent regime.

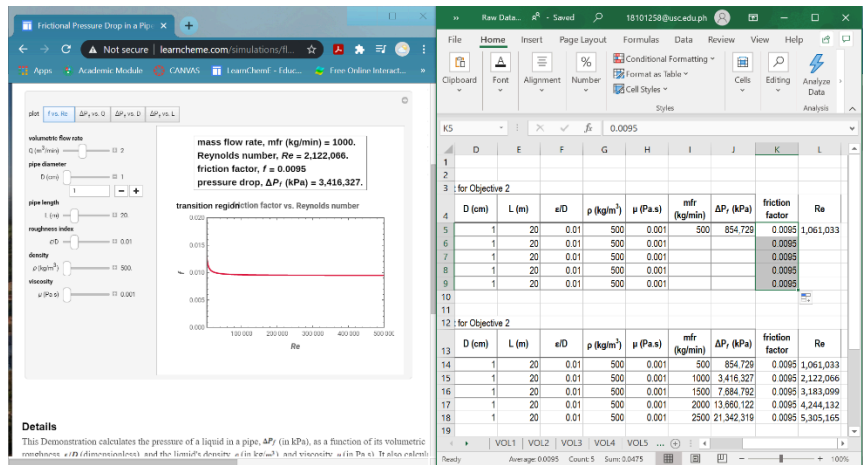
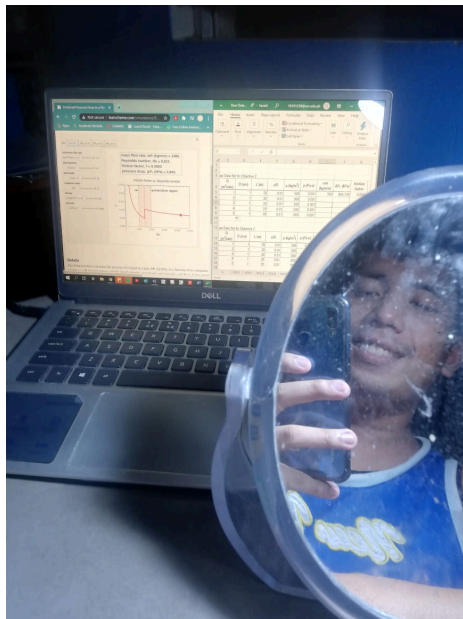


Table 1.1 Raw Data Set for Objective 1

Run	Q (m ³ /min)	D (cm)	L (m)	ϵ/D	ρ (kg/m ³)	μ (Pa.s)	Flow Regime (screenshot)	ΔP_f (kPa)	friction factor	Re
Canama	1	1	20	0.01	500	0.001		854.729	0.0095	1,061,033
Delco	1	1	20	0.01	500	0.001		854.729	0.0095	1,061,033
Talandron	1	1	20	0.01	500	0.001		854.729	0.0095	1,061,033



DELCO: Raw Data and Documentation

Table 2.1 Raw Data Set for Objective 1

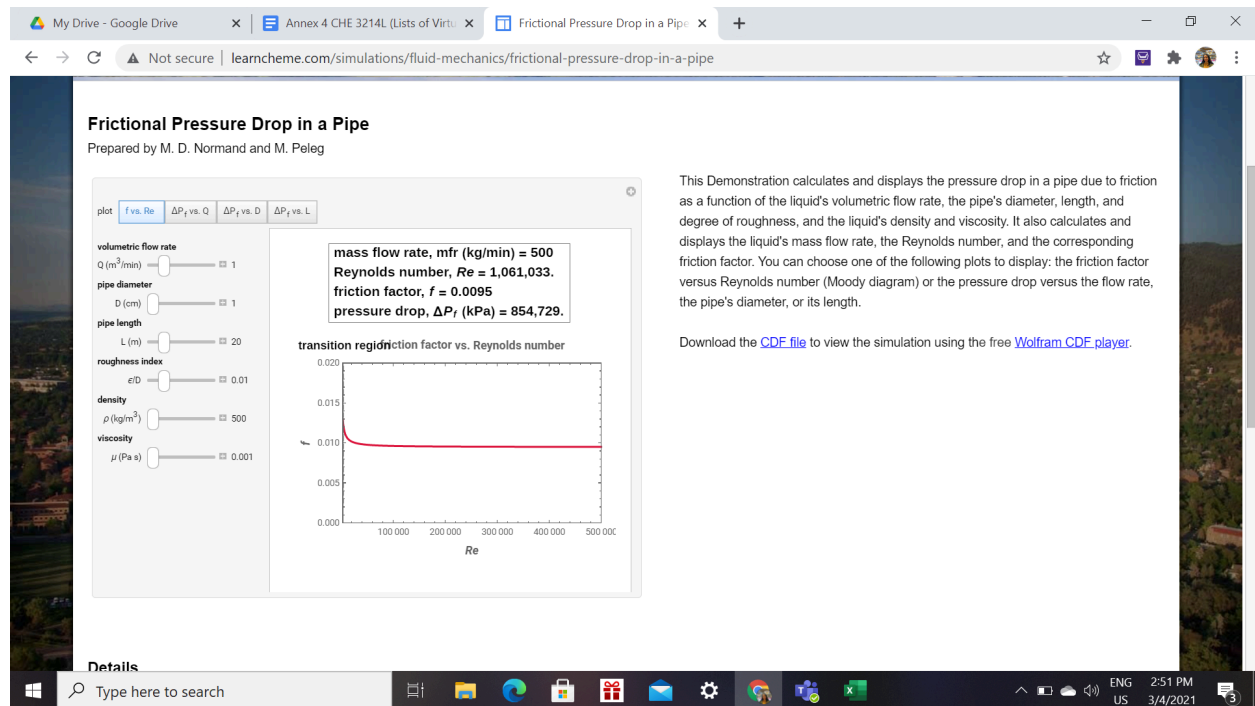
Run	Q (m ³ /min)	D (cm)	L (m)	ϵ/D	ρ (kg/m ³)	μ (Pa.s)	Flow Regime (screenshot)
1	1	1	20	0.01	500	0.001	<p>transition region friction factor vs. Reynolds number</p>
2	2	2	40	0.02	750	0.01	<p>transition region friction factor vs. Reynolds number</p>
3	3	3	60	0.03	1000	0.1	<p>transition region friction factor vs. Reynolds number</p>

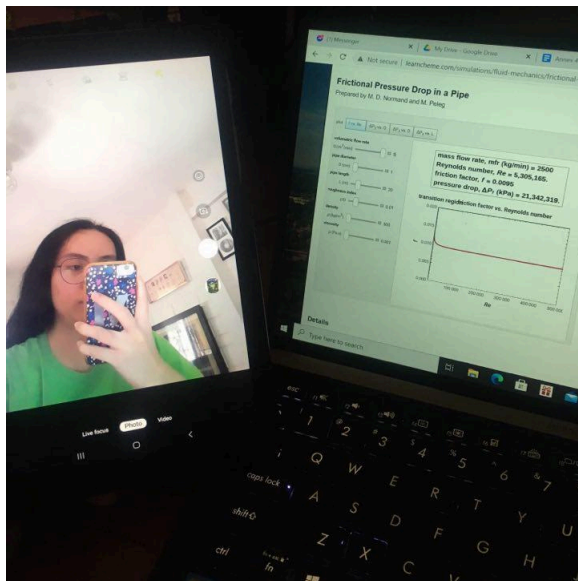
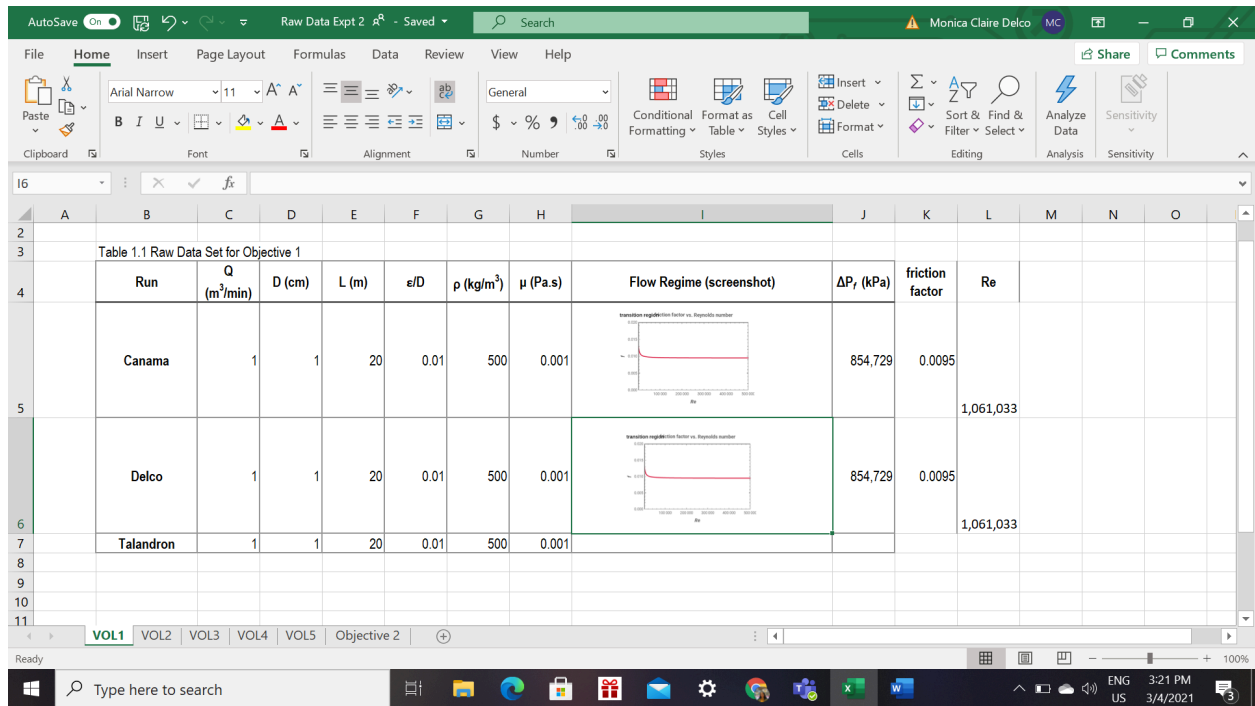
Table 2.2 Raw Data Set for Objective 2

Run	Q (m ³ /min)	D (cm)	L (m)	ϵ/D	ρ (kg/m ³)	μ (Pa.s)	mfr (kg/min)	ΔP (kPa)
1	1	1	20	0.01	500	0.001	500	854,729
2	2						1000	3,416,327
3	3						1500	7,684,792
4	4						2000	13,660,122
5	5						2500	21,342,319

Observations:

Frictional pressure drop increases as mfr increases.





TALANDRON: Raw Data and Documentation

Table 3.1 Raw Data Set for Objective 1

Run	Q (m ³ /min)	D (cm)	L (m)	ϵ/D	ρ (kg/m ³)	μ (Pa.s)	Flow Regime (screenshot)
1	1	1	20	0.01	500	0.001	<p>transition region friction factor vs. Reynolds number</p>
2	2	2	40	0.02	750	0.01	<p>transition region friction factor vs. Reynolds number</p>
3	3	3	60	0.03	1000	0.1	<p>transition region friction factor vs. Reynolds number</p>

Table 3.2 Raw Data Set for Objective 2

Run	Q (m ³ /min)	D (cm)	L (m)	ϵ/D	ρ (kg/m ³)	μ (Pa.s)	mfr (kg/min)	ΔP (kPa)
1	1	1	20	0.01	500	0.001	500	854,729
2	2						1000	3,416,327
3	3						1500	7,684,792
4	4						2000	13,660,122
5	5						2500	21,342,319

Observations:

Increasing the value of involved parameters increases the value of the pressure drop

Keeping the values of diameter, length, relative roughness, density, and viscosity constant while increasing the volumetric flowrate results to an increase in the mass flow rate

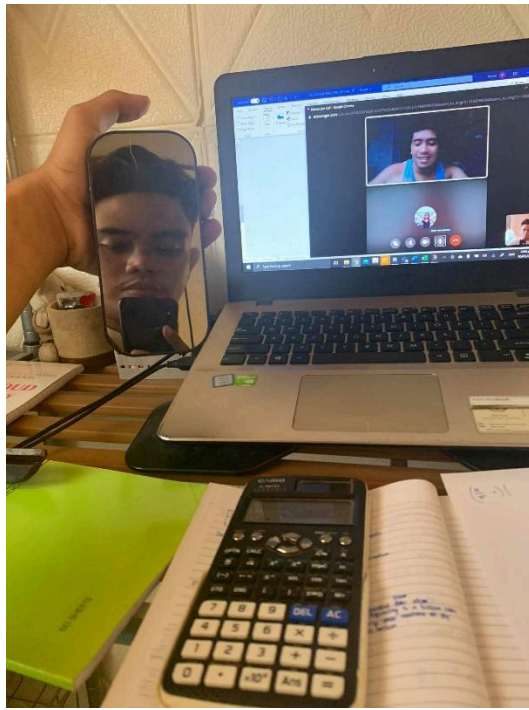
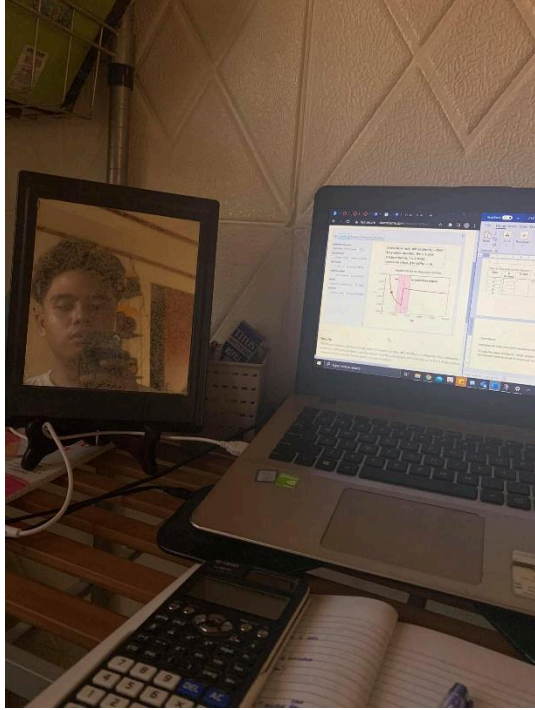
The screenshot displays a fluid mechanics simulation interface. On the left, a control panel allows adjusting parameters: volumetric flow rate Q (m³/min) at 5, pipe diameter D (cm) at 22.97, pipe length L (m) at 20, roughness index ϵ/D at 0.03, density ρ (kg/m³) at 1500, and viscosity μ (Pa s) at 0.5701. A central graph plots the friction factor f against the Reynolds number Re , showing a transition region. A text box provides calculated values: mass flow rate mfr (kg/min) = 7500, Reynolds number Re = 1,215, friction factor f = 0.0132, and pressure drop ΔP_f (kPa) = 14. On the right, a table titled 'Table 3.2 Raw Data Set for Objective 2' lists data for five runs. Below the table, an 'Observations' section contains two statements: 'Increasing the value of involved parameters increases the value of the pressure drop' and 'Keeping the values of diameter, length, relative roughness, density, and viscosity constant while increasing the volumetric flowrate results to an increase in the mass flow rate'.

Run	Q (m ³ /min)	D (cm)	L (m)	ϵ/D	ρ (kg/m ³)	μ (Pa.s)	mfr (kg/min)	ΔP (kPa)
1	1	1	20	0.01	500	0.001	500	854.729
2	2						1000	3,416.327
3	3						1500	7,684.792
4	4						2000	13,660.122
5	5						2500	21,342.319

Observations:

Increasing the value of involved parameters increases the value of the pressure drop

Keeping the values of diameter, length, relative roughness, density, and viscosity constant while increasing the volumetric flowrate results to an increase in the mass flow rate



TEAM MEETING DOCUMENTATION

Gibson



oks na atong EP?

12:13 PM

Monica



okayhan na kooo

Gibson



ang kining mass flow rate?



dili diay vol flowrate ang naa sa simulator?

Gibson



yeah pero ang obj is mass flow rate

Monica



volumetric

mon

wdym

